Lessons Learned in Magnet Slow Cooldown

Target Controls Meeting 2023-Oct-11

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UVA

Introduction

Magnet slow cooldown

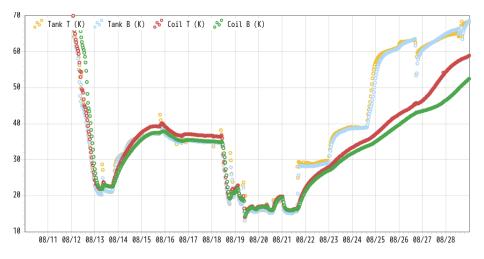
- Started on Aug. 10
- ▷ Disturbed by the LCW problem on Aug. 20-24
- ▷ Ended on Aug. 28, due to the QT stinger & HR3 problems



Elog

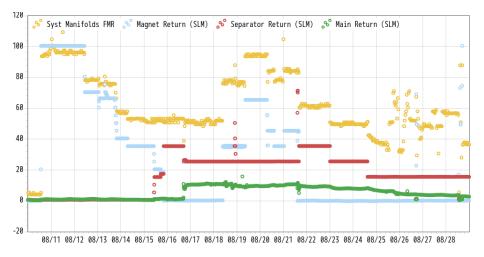
- Summary: http://twist.phys.virginia.edu:8081/General/631
- Work record: http://twist.phys.virginia.edu:8081/General/609
- Individial records; #609...658

Magnet Temperature



https://e906-gatl.fnal.gov/data-summary/e1039/target-all.php?Y0=2023&M0=8&D0=10&h0=0&m0=0&s0=0&Y1=2023&M1=8&D1=29& h1=0&m1=0&s1=0&Cryo+Temperature_Tank+T&Cryo+Temperature_Tank+B&Cryo+Temperature_Coil+T&Cryo+Temperature_Coil+B

Magnet Return Flow



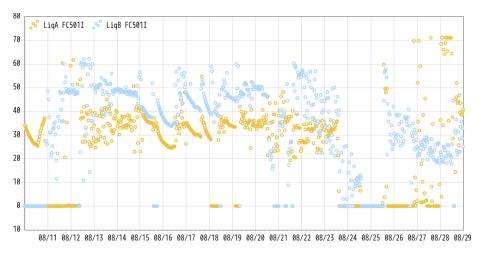
https://e906-gatl.fnal.gov/data-summary/e1039/target-all.php?Y0=2023&M0=8&D0=10&h0=0&s0=0&Y1=2023&M1=8&D1=29& h1=0&m1=0&s1=0&DLSystem0_Helium+Supply+and+Return+Manifolds+PV_FMR&Cryo+Flow_Magnet+Return&Cryo+Flow_Separator+ Return&Cryo+Flow_Main+Return

Liquefier Level



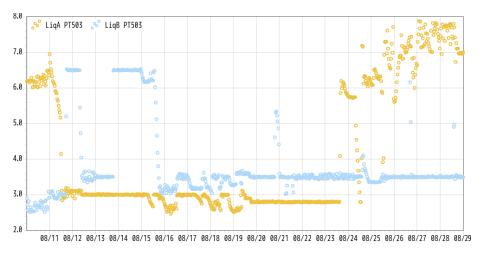
https://e906-gatl.fnal.gov/data-summary/e1039/target-all.php?Y0=2023&M0=8&D0=10&h0=0&m0=0&s0=0&Y1=2023&M1=8&D1=29& h1=0&m1=0&s1=0&DLLiqA0_Liquefier+A+PV_LI501&DLLiqB0_Liquefier+B+PV_LI501

Liquefier Inflow



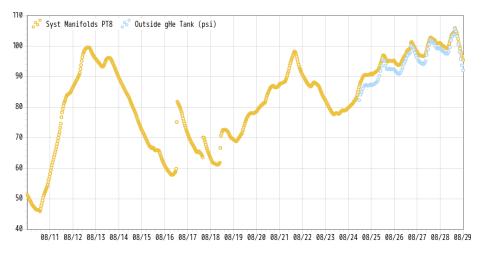
https://e906-gatl.fnal.gov/data-summary/e1039/target-all.php?Y0=2023&M0=8&D0=10&h0=0&m0=0&s0=0&Y1=2023&M1=8&D1=29& h1=0&m1=0&s1=0&DLLiqA0_Liquefier+A+PV_FC5011&DLLiqB0_Liquefier+B+PV_FC5011

Liquefier Pressure



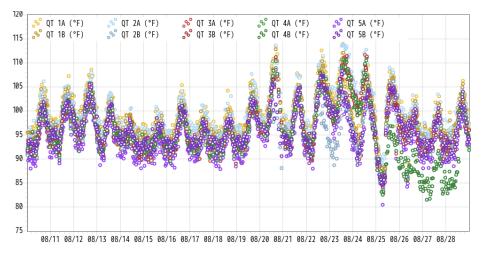
https://e906-gatl.fnal.gov/data-summary/e1039/target-all.php?Y0=2023&M0=&&D0=10&h0=0&m0=0&s0=0&Y1=2023&M1=&&D1=29& h1=0&m1=0&s1=0&DLLiqA0_Liquefier+A+PV_PT503&DLLiqB0_Liquefier+B+PV_PT503

Outside gHe Pressure



https://e906-gatl.fnal.gov/data-summary/e1039/target-all.php?Y0=2023&M0=8&D0=10&h0=0&s0=0&Y1=2023&M1=8&D1=29& h1=0&m1=0&s1=0&DLSystem0_Helium+Supply+and+Return+Manifolds+PV_PT8&Cryo+Pressure_Outside+gHe+Tank

QT LCW Temperature



https://e906-gatl.fnal.gov/data-summary/e1039/target-all.php?Y0=2023&M0=8&D0=10&h0=0&s0=0&Y1=2023&M1=8&D1=29& h1=0&s1=0&s1=0&Cryo+LCW_QT+1A&Cryo+LCW_QT+2A&Cryo+LCW_QT+3A&Cryo+LCW_QT+4A&Cryo+LCW_QT+5A&Cryo+LCW_QT+1B&Cryo+LCW_QT+2B&Cryo+2B&CF\\

List of Lessons

- 1. Sustainable flow rate
- 2. Pressure requirement for outside gHe tank
- 3. Method of using the two liquefiers seamlessly
- 4. Equilibrium temperatures at multiple flow rates
- 5. The lowest temperature with the max flow rate (150-200 SLM)
 - $^{\triangleright}\,$ No chance to try this, because of the HR3 problem.

Sustainable Flow Rate

- ► Flow rate = liquefaction rate
- ► Found to be 70 SLM in total from Liq A & B
- Expected to be 100 SLM
 - $^{\triangleright}\$ Corresponding to 4 L/h \times 2 liquefiers
 - \triangleright But the liq. rate was lower at lower pressure, as the pressure had to be as low as the magnet pressure (~3 psi)
- Remaining question
 - $^{\triangleright}~$ If we can quickly change the pressure of one liquefier that is not sending out LHe, the flow rate should be 50+35 SLM at max
 - $\triangleright \triangleright$ Should be possible once the outlet flow controller of Liq A is replaced

Pressure Requirement for Outside gHe Tank

- What is the reasonable pressure when both Liq A & B are full (200+200 L)?
- ► For conservation of He
 - $^{\triangleright}~$ 400 L of LHe in Liq A+B \Longrightarrow 100 psi when fully evaporated
 - $\,\triangleright\,\,$ The tank pressure should be ${<}20$ psi, so as to capture all evaporated He
- For liquefaction rate
 - ▷ The Liq inlet pressures (PT501A/B) drop by 30-40 psi when both Liq A & B are liquefying
 - $\,\triangleright\,\,$ The tank pressure should be 50-60 psi, so that PT501A/B are high enough to maintain the inflows
- We will be able to keep track of these relation by using the new pressure sensor next to the tank

Method of Using Two Liquefiers Seamlessly

- Using the two in parallel (simultaneously)
 - $^{\triangleright}\;$ Found to be too complicated to operate elog 635
 - One liquefier loses LHe and the other gains LHe, even when the flow rate was adjusted to keep the total level constant
 - ▷ The magnet temperature was not reproducible, namely it varied time-to-time even under the same flow rate
- Using the two in series

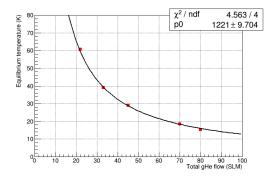
 - ▷ How long do we wait at each step, to minimize the temperature raise?
 - ▷ How much do we consume extra LHe?
 - \triangleright We didn't have a chance to quantify these, because of the HR3 problem

Equilibrium Temperatures at Multiple Flow Rates

- ▶ Model & formula elog 630
 - $Dash T = 4 + (H/(F/700*
 ho_{LHe}) L_{LHe})/S_{gHe}$ Eq. (1)
 - \triangleright T: Equilibrium temperature
 - \triangleright *H*: Total heat load (or influx), including the transfer line and the magnet
 - $\triangleright \triangleright F$: Magnet flow rate
 - $^{\scriptscriptstyle \triangleright \triangleright} ~~ \rho_{LHe} = 0.125$ kg/L: Density of LHe
 - $\texttt{PP} \ \ L_{LHe} = 2.3 \text{e4 J/kg:} \ \ \text{Latent heat of LHe}$
 - ${}^{\scriptscriptstyle \triangleright \scriptscriptstyle \triangleright} ~~ S_{gHe} = 5.2 {\rm e}3$ J/kg/K: Specific heat capacity of gHe
- Measurements elog 639 & 656
 - ▷ The eq. temperature was reproducible (i.e. one-to-one relation to flow rate) when the flow came from one liquefier (not two in parallel)
 - $\,\triangleright\,$ The eq. temperatures were measured at 22, 33, 45, 70 and 80 SLM

▶ Model fitting — elog 657

 \triangleright The measured data were fitted with Eq. (1), with *H* the only fit parameter



▷ Result; $H = 1220.6 \pm 9.7$ J/m.

It is close to the one given in doc5753 (1126 J/m = 18.7741 W).

- \triangleright Using the fit result of *H*, the minimum flow to bring the magnet to 4 K is expected to be 300 SLM
 - $rac{}{}$ F = H * 700/0.125/2.3e4 = 297 SLM
 - ▷▷ It might be different now, since we evacuate the transfer line/stinger